Development of a computational tool to predict the degradation fate of organic contaminants in **Center for** Water and Society aqueous phase advanced oxidation processes Aichigan Technological Universit Divya Kamath¹, Daisuke Minakata¹, Ph.D ¹Department of Civil and Environmental Engineering, Michigan Technological University **Challenges and Research Scope VALIDATION** of pseudo-first order rate constant (k_R) for test compound, Acetone • DIFFICULT AND EXPENSIVE TO EXPERIMENTALLY STUDY the fate of the parent compound and stable byproducts Model • Uncertainty about the **QUANTITY** and the nature of stable **BYPRODUCTS** Simplified pseudo steady • The complexity and diversity of structures of a number of known and emerging chemical **CONTAMINANTS** state **Dynamic non-**GOAL steady state We need a computational kinetic model that will "predict" the (AdOx) degradation of target organic contaminants, intermediates [HO•]ss=steady state concentration of HO• (M) and stable byproducts k'_{HO} = Second order Hydroxyl rate constant of Acetone (M⁻¹s⁻¹) Lakes, 2011) **Preliminary Results Objectives of the project** • ULTIMATE GOAL OF A KINETIC MODEL: Obtain a concentration-1) Experimental data on kinetics and byproduct time profile of the most important compounds measurement **EXPERIMENTAL**/ **Concentration-time profile from** SIMULATED CONDITIONS Pulse photolysis experiments will be conducted for kinetics and experimental results (Stefan *et al.*, 1996) measuring the resulting byproducts using mass spectrometry 1) Test compound: **ACETONE (0.001 M)** Ê 1.2 2) UV Lamp: 2) Theoretical investigations on thermodynamics $H_2O_2/10$ Medium pressure and kinetics (9 kW) 80 atior **Reverse Osmosis** UV/H_2O_2 Theoretical calculations using principles of quantum chemistry will acetate 3) Wavelength: be done to arrive at reaction barriers and reaction rate constants of oxalate 200-295 nm acetone multi-channel overall reactions 4) pH: 7 3) A predictive computational model capable of 5) [H2O2]_o : 0.015 M predicting the probable fate of degradation 60 pathways 6) Reactor Volume: Effluent time (min) 214 L Design will be based on (a) factors that account for interaction UV reactor between different species (b) Rate of the interactions (c) 0.0000300 1.6 Orientation of the resulting molecule 0.0000250 📻 Power supply $H_2O_2/10$ **S**^{1.2} **References and Acknowledgements** and lamps 0.0000200 -**Concentration-**AMERICAN WATER Minakata, Mezyk, time profile from WORKS 0.0000150 to ASSOCIATION **0.8** Jones, Daws, and dynamic non-Crittenden. ES&T steady state 0.0000100 Influent ROO• 2014, 48 (23), 13925-<u>model (AdOx™)</u> 0.4 13932 0.0000050 Ŭ **MICHIGAN SECTION Acetone**



Significance of study

• Detection of EMERGING CONTAMINANTS in drinking water sources





Contaminants such as pharmaceuticals and personal care products detected in drinking water sources (Picture source: Emerging contaminant threats and the Great

• WATER REUSE and RECLAMATION becoming a prominent Water Treatment and supply option

> Indirect potable reuse schematic in Fountain Valley, CA

Effluent from municipal wastewater treatment plant





Advanced Oxidation Process (AOP)

- An oxidation technology that mineralizes complex organic compounds when attacked by a highly reactive species called Hydroxyl Radical (HO•)
- **Rational design of AOP requires:** (a) Chemical kinetics (b) Reactor flow conditions
- Chemical kinetic modeling is the focus of this research
- Modeling kinetics of AOPs is complex because of the radical-initiated series of chain reactions

Target + HO• \rightarrow R-CH₂• \rightarrow ROO•(Peroxyl radical) \rightarrow byproducts (Carboxylic acids, aldehydes, etc.)







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Stefan, Hoy, and Bolton. ES&T, 1996, 30, 2382-2390

time (min)

80

[HO•]ss (in M)	k _R = k' _{HO} * [HO•]ss (in s ⁻¹)
4.95 x 10 -11	5.44 x 10 ⁻³
1.11 x 10 -11	1.22 x 10 -3

